

Life cycle assessment of four potable water treatment plants in northeastern Colombia

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ABSTRACT

There is currently great concern about the processes that directly or indirectly contribute to the potential for global warming, such as stratospheric ozone depletion or acidification. In this context, and provided that treated water is a basic public utility in urban centers around the world as well as in some rural areas, its impact on the environment is of great interest. Therefore, this study applied the environmental methodology of Life Cycle Assessment (LCA) to evaluate the environmental loads of four potable water treatment plants (PWTPs) located in northeastern Colombia following the international guidelines delineated in ISO 14040. The different stages of the drinking water process were thoroughly assessed, from the catchment point through pumping to the distribution network. The functional unit was defined as 1 m³ of drinking water produced at the plant. The data were analyzed through the database Ecoinvent v.3.01, and modeled and processed in the software LCA-Data Manager. The results showed that in plants PLA-CA and PLA-PO, the flocculation process has the highest environmental load, which is mostly attributable to the coagulant agent, with a range between 47-73% of the total impact. In plants PLA-TON and PLA-BOS, electricity consumption was identified as the greatest impact source, with percentages ranging from 67 to 85%. Treatment processes and techniques, bioclimatic conditions and culturally driven consumption behavior varied from region to region. Furthermore, changes in treatment processes and techniques are likely to affect the environment during all stages of a plant's operational cycle.

Keywords: climate change, environmental impact, treated water.



Avaliação do ciclo de vida de quatro estações de tratamento de água potável localizado no nordeste da Colômbia

RESUMO

Atualmente, existe uma grande preocupação com os processos que direta ou indiretamente contribuem para as alterações climáticas, destruição da camada de ozônio ou acidificação, entre outros impactos ambientais. Neste contexto, e desde que a água tratada constitui um serviço público básico em centros urbanos de todo o mundo e em algumas áreas rurais, o impacto de suas emissões no meio ambiente tem sido considerado de grande interesse. Assim, na pesquisa atual foi aplicada a metodologia ambiental de avaliação do ciclo da vida (LCA) para avaliar os impactos ambientais de quatro estações de tratamento de água potável (PWTPs), localizadas no nordeste da Colômbia seguindo diretrizes internacionais da ISO 14040. As diferentes etapas do processo de purificação a partir do ponto de captação por meio de bombeamento para a rede de distribuição foram completamente avaliadas. A unidade funcional foi definida como 1 m³ de água potável produzida na fábrica. Os dados foram analisados com base no banco de dados Ecoinvent v.3.01 e processados no software LCA-Data Manager. Os resultados possibilitaram determinar que em plantas PLA-CA e PLA -POR, o processo de floculação tem a maior carga ambiental, o que é principalmente atribuível ao agente coagulante, com uma percentagem entre 47 e 73% do impacto total. Em plantas PLA-TON e PLA-BOS, o consumo de energia eléctrica foi identificado como sendo a maior fonte de impacto, com percentagens que variam de 67 a 85%. Os processos e técnicas de tratamento, condições bioclimáticas e comportamento de consumo culturalmente impulsionado variam de região para região. Além disso, mudanças nos processos e técnicas de tratamento podem afetar o meio ambiente durante todos os estágios do ciclo de operação de uma planta.

Palavras-chave: água tratada, impacto ambiental, mudança climática.

1. INTRODUCTION

Beyond 2015, in order to fulfill the 7th objective of the Millennium Development Goals (MDGs) it will be necessary to both incorporate sustainable development principles into national policies and programs and to reduce the loss of environmental resources (United Nations, 2012).

For this purpose, it has been estimated that Colombia needs to invest approximately 4 billion dollars in order to improve unsatisfied basic needs in guaranteeing good drinking water service, which is vital to public health and human life (UNICEF, 2006). The same study revealed that, of 1027 Columbian municipalities, 70% had Potable Water Treatment Plants (PWTPs) in urban areas and 20% in rural areas.

These PWTPs are typically supplied by surface waters (mainly rivers) and utilize gravity, pumping and/or mixed systems to move the water from the catchment point, where the first stage of the drinking water process occurs. Subsequently, a series of conventional methods are applied, consisting of a more or less standardized sequence of physicochemical and, sometimes, biological treatment processes which vary depending on the quality of the water that enters the plant (Stackelberg et al., 2007). These processes require energy and chemical supplies in order to guarantee an adequate product for human consumption (Friedrich 2002).

However, excessive power consumption or use of chemical agents such as coagulants, flocculants, pH stabilizers and disinfectants not only impact consumer health, but generate environmental loads as well (Khan et al., 2013; Mery et al., 2013; Ribera et al., 2014). This has generated significant social and industrial interest in developing new strategies aimed at



improving environmental indicators throughout the entire water management life cycle (Vince et al., 2008; Amores et al., 2013), and at obtaining cleaner and more sustainable processes in order to provide a better quality of life for the consumer of the final product (El-Sayed Mohamed et al., 2010).

Environmental methodologies such as Life Cycle Assessment (LCA), which follows ISO 14040 guidelines (ISO, 2006), allow assessing the environmental loads generated by a process and/or product during its life cycle, with the aim of reducing environmental loads, thereby improving sustainability indicators.

The scientific literature on water science and technology includes important international studies which have applied LCA during the last five years. These studies have increasingly gained more attention as they have been applied to the processes of potable water treatment plants in developed and developing countries (Kulay et al., 2015; Ahmadi and Tiruta-Barna 2015; Bonton et. al., 2012; Hyunju et al., 2015; Igos et al., 2013; Meneses et al., 2010; Pasqualino et al., 2011; Ribera et al., 2014).

During this decade in Latin America, countries such as Argentina, Brazil, Colombia and Mexico have been making progress in the application and capacity building of LCA in different economic sectors. Although this application has included both private companies and governments, it must still develop specifically targeted programs as well as financial support and technical assistance, in order that it may become a fundamental policy and, as such, the cornerstone of any industrial process (Güereca et al., 2015; Swarr et al., 2015).

The current research therefore constitutes one of the first applications of LCA to PWTPs in Colombia. As such, it represents a significant contribution to the domain of water science and technology in fostering the use of LCA in developing countries, using a combination of promotion among both natural science and engineering experts. In this context, the main objective of the present research was to apply LCA to four PWTPs located in northeastern Colombia and, based upon the results, propose strategies that allow mitigating the environmental impact of the potable water processes currently used in these PWTPs.

2. METHODOLOGY

The LCA methodology consists of four stages (Ortiz-R et al., 2014):

2.1. Objective definition and scope

This stage defines the limits of the system and the level of detail of the study. The four studied PWTPs are located in northeastern Colombia and deliver potable water to approximately 4 million inhabitants. These plants were selected from the municipal development plans. They are located in different cities and each one draws water from different catchment points. Due to confidentiality concerns, the PWTPs are labeled hereafter as plant PLA-CA, PLA-POR, PLA-TON and PLA-BOS, respectively. Each plant was analyzed in terms of the different stages of the drinking water process, (e.g. catchment point, de-sanding, coagulation, flocculation, sedimentation, filtration, disinfection, storage before the distribution network). A general scheme of the four PWTPs is shown in Figure 1.

For example, PLA-CA (i) has a pretreatment process meanwhile PLA-POR (ii), PLA-TON (iii) and PLA-BOS (iv) complete the flocculation process by using hydraulic and mechanical systems. For all cases, the water source was surface water with levels of turbidity equal to 6.58 NTU (Nephelometric Turbidity Unit), Dissolved Oxygen (DO) 4.8 mg L⁻¹, pH 7.67, BOD 5 2.38 mg L⁻¹, COD 4,34 mg L⁻¹, uncountable bacteriological pollution. All values were considered according to the Colombian national standard (Colombia, 2000).

In this context, the data collected were quantitatively related to one quantitative output of the product. In this research, the functional unit is defined as "1 m^3 of drinking water





produced at the plant".

Figure 1. System boundaries of the process at the PWTPs studied.

The following assumptions were considered:

• Electric power generation corresponds to an energetic mix of 78% hydro-electrical plants, 7% carbon, 12% gas and 3% other sources, adapted from Ortiz-R and García-Cáceres (2013).

• Environmental loads due to the maintenance of the sedimentation zone have been calculated using sodium hypochlorite and tap water.

• The infrastructure was assumed to last 50 years.

Transportation of coagulants and other reagents was not considered. It was assumed that these raw materials are disposed of at the plant. Also, the distribution network has not been included in this research. The transportation and distribution phases will be included and discussed in future studies.

2.2. Inventory analysis

This stage developed an inventory of inputs and outputs of the water treatment system based not only on information regarding power consumption and chemical supplies required in the drinking water process, but on the equivalent contaminating factor as well. Both primary and secondary information sources were employed for this inventory.

The primary source corresponded to data provided by the technical personnel of the studied plants, who collected information about the plants' processes during an operational period of twelve (12) months, from January to December of 2014. The secondary source corresponded to the database Ecoinvent v3.01(Ecoinvent, 2013), which was intended to provide background generic data about the products and processes employed in the PWTPs. Table 1 shows the inventory of chemical supplies and energy flow at each of the studied plants.

2.3. Impact assessment

This stage provided the environmental indicators which supported the assessment of the Life Cycle Inventory (LCI) results. The CML 2001 method was chosen in the present research because it provides operational guidelines for conducting an LCA study step by step according to the ISO standards according to Guinée (2002). This method is a midpoint approach which covers all emissions and resource-related impacts (e.g. carbon dioxide,



produced at the plant.								
		Plant 1	Plant 2	Plant 3	Plant 4			
Process	Input	Amount per FU						
Disinfection with Chlorine	Chlorine gas (kg m ⁻³)	1.64E-03	1.84E-03	1.41E-03	2.61E-03			
	Clarifloc (Coagulant: kg m ⁻³)	1.65E-02	-	-	-			
Coagulation	Aluminum sulfate (kg m ⁻³)	-	-	-	4.45E-02			
	Coagulant AK 23 (kg m ⁻³)	-	6.83E-03	4.09E-03	-			
Coagulation Flocculation	Super Floc (Polymer: kg m ⁻³)	-	9.00E-05	9.80E-05	1.79E-04			
pH Stabilization and Pretreatment	Hydrated lime (kg m ⁻³)		-	-	8.49E-05			
Flocculation and distribution network	Mechanical Flocculators and drive pumps <u>(</u> kWh m ⁻³)	-	1.37E-02	6.20E-01	1.31E+00			

methane, N_2O and other greenhouse gas emissions were aggregated into CO_2 equivalent emissions in accordance with their respective global warming potential).

Table 1. Inventory of the four PWTPs expressed in the functional unit (FU) "1 m³ of drinking water produced at the plant.

In the present research, Global Warming Potential (GWP) (kg CO₂-Eq) was chosen as the main environmental impact because of its worldwide effect, which makes it the greatest environmental challenge presently facing the sustainable water management of the world (Russo et al., 2014). Some other environmental impacts corresponded to acidification (kg SO_2 -Eq), and stratospheric ozone depletion (SOD/kgCFC-11-Eq). Finally, the software LCA-Data Manager® (an environmental management tool developed by SIMPPLE S.L.) was used to create and modify the scenarios under study as well as to develop the material balances and the inventory (SIMPPLE SL, 2013).

2.57E-03

2.4. Interpretation of results

Maintenance in the

filtration

The last stage is the interpretation of the results, not only in terms of environmental load assessment, but also through the generation of alternative proposals for mitigating the environmental impacts associated with the process (Ortiz-R et al., 2010).

3. RESULTS AND DISCUSSION

Energy Consumption

 $(kWh m^{-3})$

Table 2 presents the overall results obtained by applying the environmental impact indicators to the four studied plants. The results show a similar order of magnitude to those reported by Amores et al., (2013) and Ribera et al. (2014) in terms of the application of aluminum sulfate and chlorine gas to the drinking water process. It can also be observed that PLA-BOS has the highest impact of all of the environmental impacts studied. With respect to GWP, this plant emitted indirect emissions of 3.83E-01 kg CO₂-Eq, of which 86% corresponded to extended power consumption during the pumping process, mainly due to the topographic conditions of the plant's location. This was also the case for the elevated water



volumes forced by the use of the chemical agents required for the flocculation and disinfection processes. Contrastingly, the plant that emitted the least emissions was PLA-TON, with 1.39E-02 kg CO₂-Eq, resulting from low energy consumption and from the particular nature of the treated hydric source. In effect, water in this case only needs to travel a short distance from its source to the catchment point, thus accounting for the low potable water chemical agent requirements of this plant.

Environmental Indicator	PLA-CA	PLA-TON	PLA-POR	PLA-BOS
Abiotic resource depletion (kg Antimony eq)	1.39E-04	8.06E-05	6.11E-04	1.46E-03
Acidification potential (kg SO2 eq)	2.28E-04	1.12E-04	5.90E-04	1.48E-03
Eutrophication (kg PO ₄ eq)	5.03E-05	3.16E-05	1.93E-04	5.05E-04
Global warming potential (kg CO ₂ eq)	2.21E-02	1.39E-02	1.73E-01	3.83E-01
Stratospheric ozone depletion (kg CFC-11 eq)	4.14E-09	3.22E-09	9.56E-09	2.23E-08
Human Toxicity (kg 1,4-DCB eq)	8.04E-03	4.72E-03	4.31E-02	9.81E-02

Table 2. Results of the environmental impact assessments of the four potable water treatment plants.

Previous results show that in PLA-CA and PLA-TON the highest impact was due to the use of the coagulant agent, respectively accounting for 82% and 46% of the total impact of each of these plants. The second greatest impact in these plants was caused by chlorine gas, which is employed in the disinfection process, with total emission percentages of 13% and 21% for PLA-CA and PLA-POR, respectively. Energy consumption contributed 4% in PLA-CA, resulting from processes like pumping, flocculation and filter re-washing (locally named retrolavado). In PLA-POR, power consumption accounted for 30% of total emissions, while 3% was attributed to a polymer employed as coagulation coadjutant. Regarding PLA-TON, the greatest impact was due to energy consumption, since the plant uses a water suction supply system. This was also the case with PLA-BOS, where the use of monitoring systems, flocculation, engines (moto-redactors), compressors for the pneumatic gates system, and electric drive pumps was found to emit 2.83E-01 kg CO₂ eq., all of which makes up 92% of the total emissions relating to GWP. Such an elevated percentage results from the need to move large volumes of water and the unfavorable location of the plant with respect to the population it services. The emissions of both PLA-TON and PLA-BOS are less intense due to the application of coagulant substances such as AK23 and aluminum sulfate, which respectively accounted for 1% and 7% of total emissions (Figure 2).



Figure 2. Percentages affecting Global Warming based on 1 m³ of drinking water produced at the plant.

Regarding the environmental impact of GWP, CO_2 emissions resulting from fossil fuel combustion cause the greatest impact on the atmosphere. Ethane (HFC) accounted for 3 to 18% of total GEGs (Greenhouse Effect Gases) (Figure 3).



Figure 3. Total of GEG percentages based on 1 m³ of drinking water produced at the plant.

The compared effects of the studied plants across environmental impacts shows a basic trend, according to which PLA-BOS has the greatest impact, followed by PLA-CA and PLA-TON, while the smallest impact corresponds to PLA-POR. However, in the case of ozone layer depletion, the latter three plants exhibit close values.

The largest environmental impact due to contaminant additives corresponded to the use of chlorine gas in PLA-CA and PLA-POR, with 79% and 89% of the overall impact, respectively. The second largest impact was caused by the coagulant agent Clarifloc, which was applied in PLA-CA and accounted for 21% of the overall impact, and by the coagulant agent AK23, used in PLA-POR, where it generated 9% of said impact.

In PLA-CA, the largest impact was caused by Clarifloc (82%), followed by chlorine gas (13%) and energy consumption (4%). In PLA-POR, the largest impact corresponded to AK23 (46%), followed by electricity consumption (30%), chlorine gas (21%) and polymer addition (3%). Contrastingly, the most outstanding impact in PLA-BOS was electricity consumption, with 92%, followed by aluminum sulfate (7%) and chorine gas (0.18%). Finally, energy consumption also dominated in PLA-TON, with 74%, contrasting with the low counts registered by the other environmental impacts.

These indicators reveal that there are processes and energy flows in each of these plants that have indirectly adverse environmental effects. For this reason, the companies involved in the sustainability of the drinking water service should ideally reduce these environmental loads during the entire process.

For example, the use of Clarifloc can be reduced by applying coadjutants or other coagulant agents. Also, the preservation of the hydric source that supplies the treatment plant is an important factor, since its deterioration contaminates the water that is to be treated. This contamination involves color, turbidity and suspended material, all of which directly affect the amounts of coagulant that are needed to purify the water. The best scenario might be reached by analyzing the viability of a pretreatment process intended to improve the physicochemical characteristics of the water that enters the plant, thus reducing the need for coagulant.

As to the application of chlorine gas, there are alternatives such as inverse osmosis (Vingerhoeds et al., 2016), nanofiltration (Shon et al., 2013), UV disinfection, per acetic acid and advanced oxidative processes such as the PAA/UV (De Souza et al., 2015) which



eliminate all pathogens. This is likely to reduce the application of chlorine to the residual dose stipulated by the corresponding Colombian normative system through Resolution 2115 of 2007. Yet this alternative also has disadvantages, since it requires higher investments and power consumption during the process of membrane filtration (Villamizar et al., 2015).

In those PWTPs producing unfavorable impacts due to the use of the coagulant agent, environmental loads can be reduced by 5-20% by analyzing the necessary dose. For example, pilot tests can be conducted to assess the efficiency of the coagulant as compared to that of other substances with weaker environmental impact. It is also possible to reduce the use of coagulant by introducing flocculation coadjutants with better performance than the polymers currently employed. The effect of increasing the polymer dose in order to reduce the necessary amount of coagulant may also be studied.

Finally, regarding elevated power consumption due either to water transport over long distances (from the catchment point to the plant, from the plant to the distribution network, or from any point to altitudes above 200 m from where the plant is located) or processes such as flocculation, more efficient energy alternatives must be considered.

4. CONCLUSIONS

In this study, we applied LCA to four PWTPs located in northeastern Colombia. In conclusion, it can be said that the use of Clarifloc can be reduced by applying coadjutants or other coagulant agents. Also, the preservation of the hydric source that supplies the treatment plant is an important factor, since its deterioration contaminates the water that is to be treated. Treatment processes and techniques, bioclimatic conditions and culturally driven consumption behavior vary from region to region. Furthermore, changes in treatment processes and techniques are likely to affect the environment during all stages of a plant's operational cycle. Therefore, any improvement is generally oriented to raw materials and energy use, always keeping in mind that a treatment plant must be both environmentally and socio-economically feasible. The different types of treatment techniques vary substantially depending on the geographic location of the plant.

Climate, technological, cultural and socio-economical differences clearly define a plant's standards in any context and region. However, the function is always the same: providing good water quality for the people it serves. To a great extent, variations in results are due to the different conditions under which the process is conducted. One of the most important variables is the hydric source that supplies the plant, depending on the particular supply types and amounts may be used in the potable water process.

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